

Condenser Revamping

Specifically adapted for the modular renovation of steam surface condensers through complete replacement of the tube bundles, this program calculates the performance of the new unit and corresponding production gains for a one year period from turbine and cooling water pump characteristics.

This program is intended for carrying out perform optimization studies of thermoelectric plant steam condenser tube bundles to facilitate bundle replacement in modular systems whereby existing tube bundles are exchanged for an alternative design with different geometric characteristics including tube type and quantity. So the program is designed to be used by equipment manufacturers who want to participate in the market of condenser revamping. But the program can also be of use to the thermoelectric plant owners since it can be used to carry out a performance analysis of condensers.

Modular revamping of condensers is a technique that has been employed for many years and was originally developed in response to the need to change the material of the tubes because of degradation and to avoid the denting phenomenon which can occur in the steam generators of nuclear systems containing condensers with copper alloy tubing.

The modular revamping of a condenser may call for use of a different tube material, tube diameter and tube quantity, making it necessary to perform a hydraulic study of the available pumping capacity. At the same time, the new tube bundle should be adapted to the characteristics of the bundle location in the shell of the condenser whilst aiming to improve the unit efficiency by increasing the installed heat transfer surface area.

With this program one can carry out this study as well as evaluate the efficiency of the unit during the course of its operating lifetime by means of the turbine and refrigeration system conditions.

Currently, the renovation of these condensers, due to the problems associated with the use of copper, is diminishing owing to the fact that new units already incorporate tubes of more resistant materials and have improved design efficiencies.

Nevertheless, the use of this program is not limited to revamping studies of this nature, but rather, the program can be used to study the performance of an existing condenser and then compare this with a hypothetical newly renovated condenser.

In the same way, if the condenser performance is decreasing, the program can be used to verify the loss of efficiency of the unit in relation to the performance of the condenser when it was installed.

The following section includes a description of the program, how to use it and how to interpret the calculated results.

Before starting the program the user should confirm that they possess the required geometry and process data, the latter of which should reflect the characteristics observed at the plant, specifically the cooling water pumping curve, the turbine efficiency curve in function of the condenser vacuum and the temperatures of the cooling water at the time of the evaluation.

After starting the program, the initial screen shows the Input Sheet where the required data, corresponding to the existing condenser, are specified by the user. There are three data that may be unfamiliar. Firstly, the level difference between the suction and propulsion of the pump. This information should be provided by the unit owner. Secondly, the maximum insertion dimensions for the new tube bundle. This information should be gleaned from plans of the existing condenser and its surroundings, with the aim of maximizing the installed heat transfer surface. Thirdly, the tube occupation coefficient, which is the relationship between the drilled area of the tubesheet for placement of the tubes and the total tubesheet area (width by height).

For new condensers, it is necessary to specify the following data:

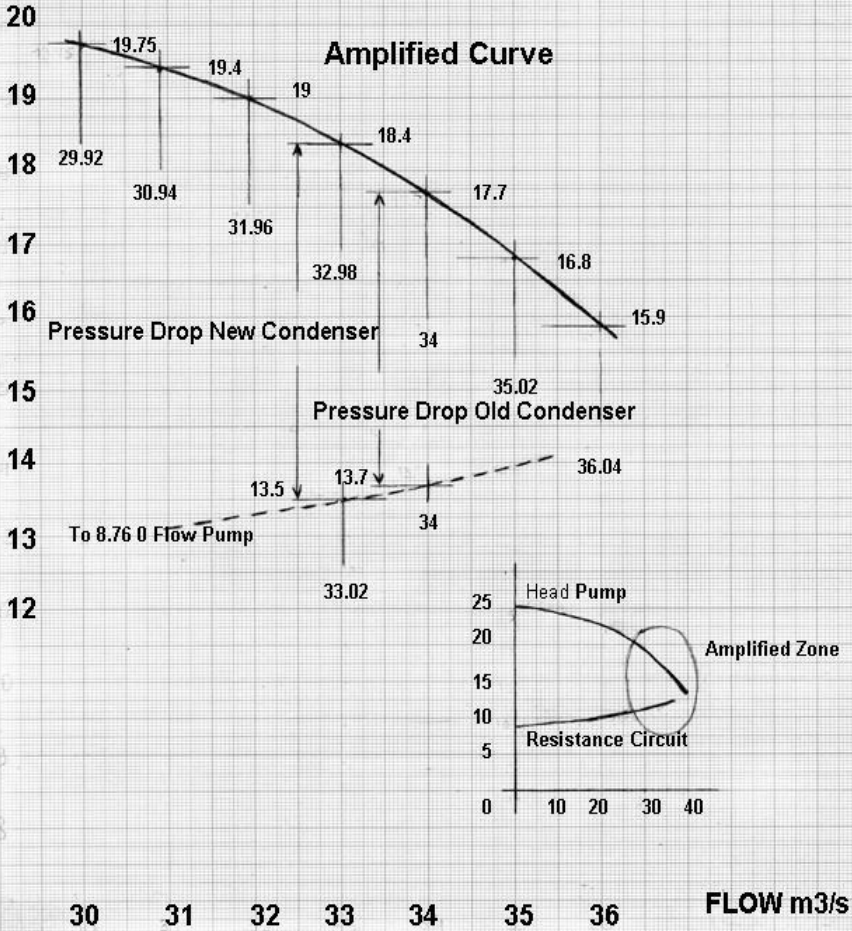
- The specified inside diameter of the tubes for the first calculation should be similar to the inside diameter of the existing tubes and this can then be modified later depending on the desired result.
- The tube length will be, except in rare cases, the same as the existing length.
- The number of tube bundles will be, naturally, the same as the existing number.
- The tube occupation coefficient is fundamental, as this determines the final number of tubes. One should perform an advance study of this coefficient with relation to the dimensions of the new tubesheets bearing in mind that according to experience this coefficient is typically around 0.35 for low density bundles and 0.45 for very compact bundles but with an elevated risk of not complying with the available pressure drop in the body of the condenser.
- Exchange coefficients are according to H.E.I. (Heat Exchange Institute).
- The rest of the data are self-explanatory except for the cleanliness coefficient which can be greater than 1 in simulation with materials other than titanium or stainless steel which are the materials considered by this program and those most commonly considered in modular revamping projects. This coefficient can also be employed to simulate the deterioration in performance of condensers.

Example Pump Performance Curve



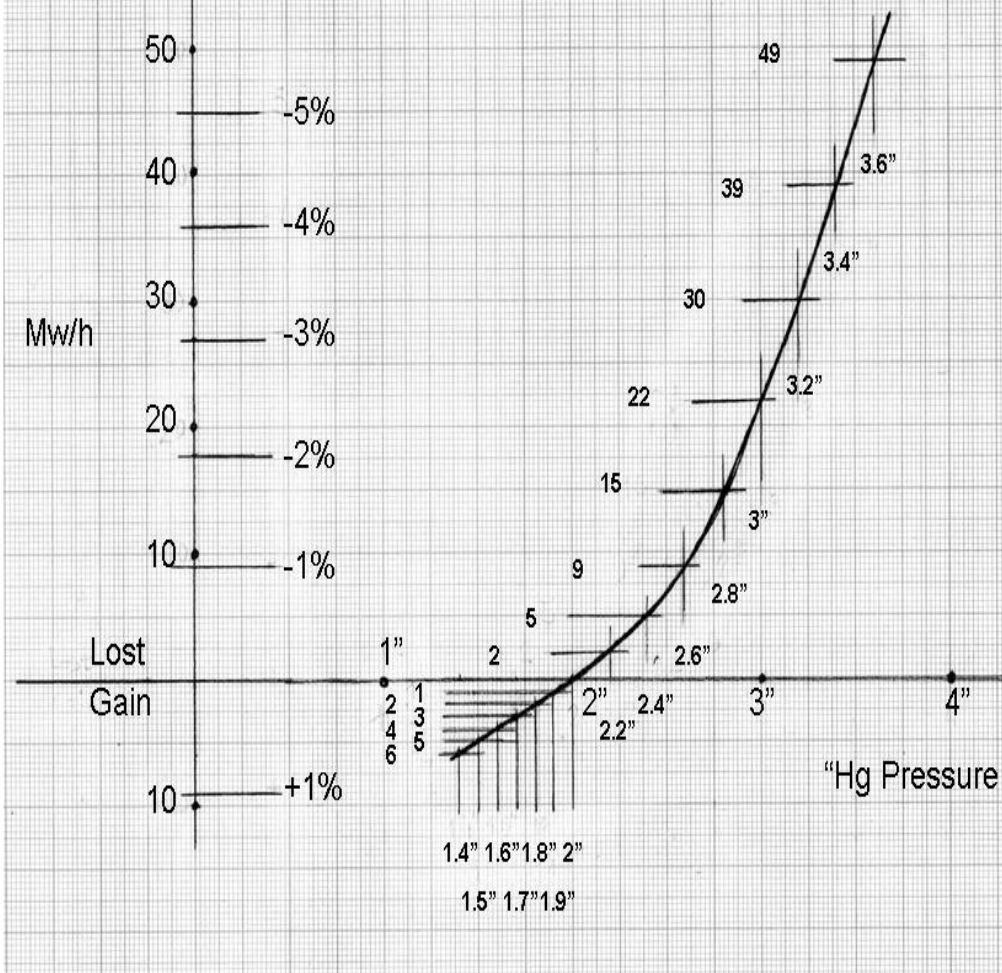
ASC Example

HEAD PUMP

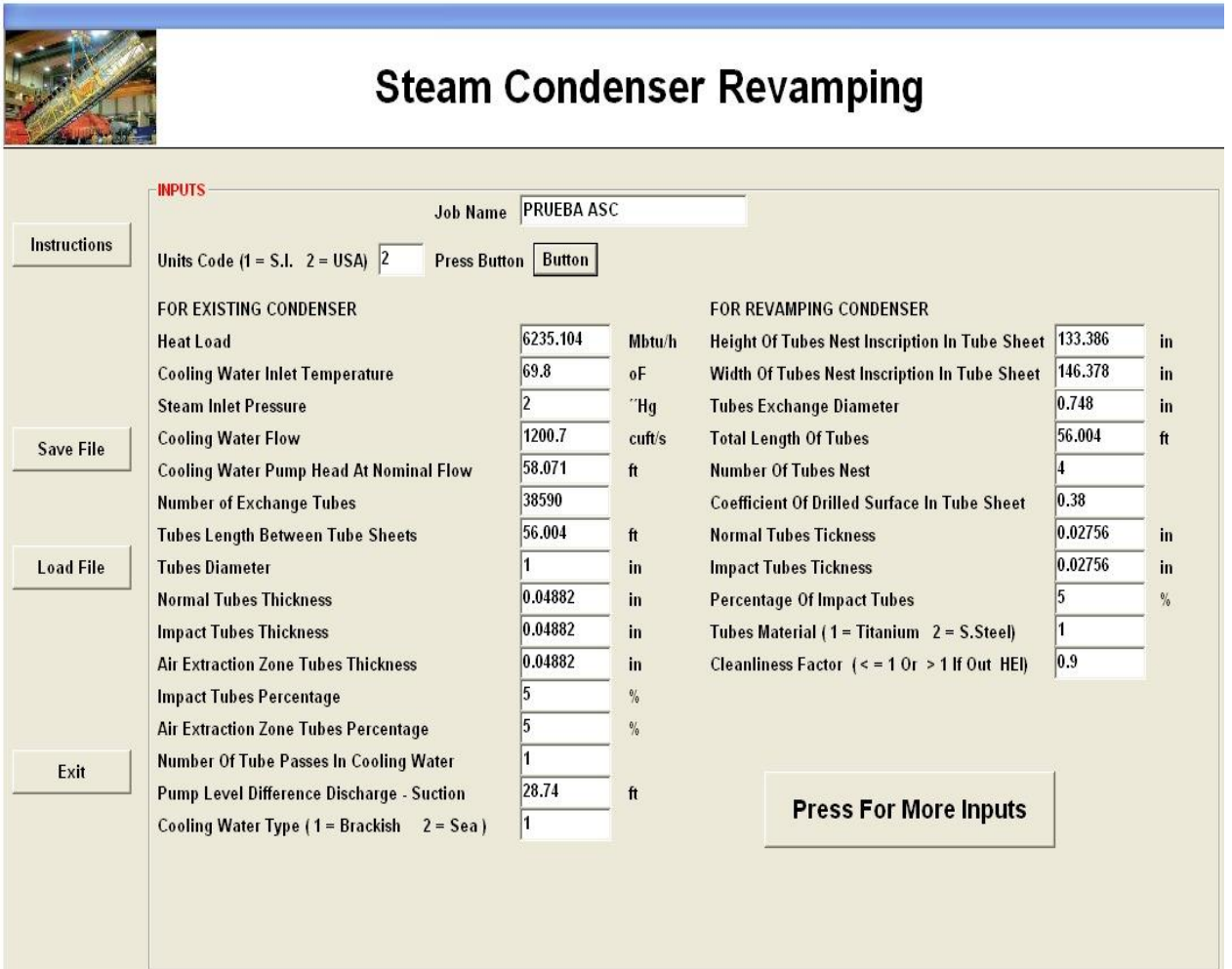


TURBINE EFFICIENCY (900 Mw/h)

Mw/h (Gain-Lost) versus Condenser Pressure



PROGRAM WINDOWS



Steam Condenser Revamping

INPUTS

Job Name: PRUEBA ASC

Units Code (1 = S.I. 2 = USA): 2 Press Button: Button

FOR EXISTING CONDENSER			FOR REVAMPING CONDENSER		
Heat Load	6235.104	Mbtu/h	Height Of Tubes Nest Inscription In Tube Sheet	133.386	in
Cooling Water Inlet Temperature	69.8	oF	Width Of Tubes Nest Inscription In Tube Sheet	146.378	in
Steam Inlet Pressure	2	"Hg	Tubes Exchange Diameter	0.748	in
Cooling Water Flow	1200.7	cuft/s	Total Length Of Tubes	56.004	ft
Cooling Water Pump Head At Nominal Flow	58.071	ft	Number Of Tubes Nest	4	
Number of Exchange Tubes	38590		Coefficient Of Drilled Surface In Tube Sheet	0.38	
Tubes Length Between Tube Sheets	56.004	ft	Normal Tubes Tickness	0.02756	in
Tubes Diameter	1	in	Impact Tubes Tickness	0.02756	in
Normal Tubes Thickness	0.04882	in	Percentage Of Impact Tubes	5	%
Impact Tubes Thickness	0.04882	in	Tubes Material (1 = Titanium 2 = S.Steel)	1	
Air Extraction Zone Tubes Thickness	0.04882	in	Cleanliness Factor (< = 1 Or > 1 If Out HEL)	0.9	
Impact Tubes Percentage	5	%			
Air Extraction Zone Tubes Percentage	5	%			
Number Of Tube Passes In Cooling Water	1				
Pump Level Difference Discharge - Suction	28.74	ft			
Cooling Water Type (1 = Brackish 2 = Sea)	1				

Buttons: Instructions, Save File, Load File, Exit, Press For More Inputs

DATA ENTRY WINDOW 1/2



Steam Condenser Revamping

Run File	INPUTS			GAIN IN MW/H AT CURVE VACUUM PRESSURE VERSUS EFFICIENCY			
	AVERAGE COOLING WATER TEMPERATURE IN °F PER MONTH (First Temperature Must Be Design Temperature Of The Unit)			Mw/h Gain At	1,399	"Hg Pressure	<input type="text" value="6"/>
	Average C.W. Temperature In January			Mw/h Gain At	1,5	"Hg Pressure	<input type="text" value="5"/>
	Average C.W. Temperature In February			Mw/h Gain At	1,6	"Hg Pressure	<input type="text" value="4"/>
	Average C.W. Temperature In March			Mw/h Gain At	1,699	"Hg Pressure	<input type="text" value="3"/>
	Average C.W. Temperature In April			Mw/h Gain At	1,8	"Hg Pressure	<input type="text" value="2"/>
	Average C.W. Temperature In May			Mw/h Gain At	1,9	"Hg Pressure	<input type="text" value="1"/>
	Average C.W. Temperature In June			Mw/h Gain At	2	"Hg Pressure	<input type="text" value="0"/>
	Average C.W. Temperature In July			LOSS IN MW/H AT CURVE VACUUM PRESSURE VERSUS EFFICIENCY			
	Average C.W. Temperature In August			Mw/h Loss At	2	"Hg Pressure	<input type="text" value="0"/>
Results	Average C.W. Temperature In September			Mw/h Loss At	2,2	"Hg Pressure	<input type="text" value="2"/>
	Average C.W. Temperature In October			Mw/h Loss At	2,399	"Hg Pressure	<input type="text" value="5"/>
	Average C.W. Temperature In November			Mw/h Loss At	2,6	"Hg Pressure	<input type="text" value="9"/>
	Average C.W. Temperature In December			Mw/h Loss At	2,799	"Hg Pressure	<input type="text" value="15"/>
	HEAD OF PUMP AT COOLING WATER FLOW (FOOT)			Mw/h Loss At	3	"Hg Pressure	<input type="text" value="22"/>
	Pump Head At C.W. Flow Of 1056,62 cuft/s			Mw/h Loss At	3,2	"Hg Pressure	<input type="text" value="30"/>
	Pump Head At C.W. Flow Of 1092,64 cuft/s			Mw/h Loss At	3,399	"Hg Pressure	<input type="text" value="39"/>
	Pump Head At C.W. Flow Of 1128,66 cuft/s			Mw/h Loss At	3,6	"HG Pressure	<input type="text" value="49"/>
	Pump Head At C.W. Flow Of 1164,68 cuft/s			HOURS PER MONTH PRODUCING AT 100% LOAD			
	Pump Head At C.W. Flow Of 1200,7 cuft/s			Hours In January	<input type="text" value="700"/>		
Pump Head At C.W. Flow Of 1236,72 cuft/s			Hours In February	<input type="text" value="700"/>			
Pump Head At C.W. Flow Of 1272,74 cuft/s			Hours In March	<input type="text" value="700"/>			
Print Results				Hours In April	<input type="text" value="700"/>		
				Hours In May	<input type="text" value="700"/>		
				Hours In June	<input type="text" value="700"/>		
				Hours In July	<input type="text" value="700"/>		
				Hours In August	<input type="text" value="700"/>		
				Hours In September	<input type="text" value="700"/>		
				Hours In October	<input type="text" value="700"/>		
				Hours In November	<input type="text" value="700"/>		
				Hours In December	<input type="text" value="700"/>		
Save File							
Load File							
To First Page							
Exit							

DATA ENTRY WINDOW 2/2



Steam Condenser Revamping - Results 1/2

Job Name : PRUEBA ASC

TEMP = C.W.Temperature (oF) COEFF = Exchange Coefficient (Btu/hoFft2)
 INCRE = C.W.Increase Temperature (oF) FLOW = Cooling Water Flow (cuft/s)
 COND = Condensation Temperature (oF) PRES = Condensation Pressure (" Hg)
 VELO = Tubes Velocity (ft/s) DROP = Tube Side Pres.Drop (wftc) MW = Gain or Loss (Mwh)

TEMP	COEFF	INCRE	FLOW	VELO	DROP	COND	PRES	MWh
69,8	567,1	23,77	1166,72	6,59	16,07	99,62	1,911	619,2
71,6	572,5	23,76	1167,33	6,6	16,02	101,3	2,009	-71,8
75,2	582,1	23,73	1168,7	6,6	15,91	104,68	2,223	-1671,4
77	586,3	23,72	1169,32	6,61	15,86	106,39	2,337	-2866,9
62,6	539,9	23,83	1163,87	6,58	16,31	93,09	1,565	3035,9
64,4	547,6	23,82	1164,61	6,58	16,25	94,69	1,644	2478,6
66,2	554,7	23,8	1165,35	6,58	16,19	96,31	1,729	1889,8
68	561,1	23,79	1165,97	6,59	16,13	97,97	1,817	1267,3
59	522,7	23,87	1162,25	6,57	16,43	89,94	1,419	4059,6
60,8	531,6	23,85	1163,12	6,57	16,37	91,5	1,49	3562,7
71,6	572,5	23,76	1167,33	6,6	16,02	101,3	2,009	-71,8
68	561,1	23,79	1165,97	6,59	16,13	97,97	1,817	1267,3

Gain or Loss (-) in Mwh 13499,1

Press For Results 2/2

RESULTS SHEET 1/2



Steam Condenser Revamping - Data And Results 2/2

Job Name : PRUEBA ASC

■ Data For Existing Condenser

Total Heat Load	6235,104	Mbtuh
Cooling Water Inlet Temperature	69,8	oF
Design Pressure	2	" Hg
Cooling Water Flow	1200,7	cuft/s
Pump Head Design Cooling Water Flow	58,071	ft
Total Number Of Tubes	38590	
Total Length Of Tubes	56,004	ft
Diameter Of Tubes	1	in
Normal Tubes Thickness	0,04882	in
Impact Tubes Thickness	0,04882	in
Air Cooling Zone Tubes Thickness	0,04882	in
Impact Tubes Percentage	5	%
Air Cooling Zone Tubes Percentage	5	%
Cooling Flow Passes	1	
Pump Level Differen.Discharge - Suction	28,74	ft
Cooling Water Type	Brackish Water	

■ Data For Condenser Revamping

Height Of Tube Nest Inscrip.Tube Sheet	133,386	in
Width Of Tube Nest Inscrip.Tube Sheet	146,378	in
Tubes Diameter	0,748	in
Length Of Tubes	56,004	ft
Number Of Tubes Nest	4	
Drilled Surface Coeffic. In Tube Sheet	0,38	
Normal Tubes Thickness	0,02756	in
Impact Tubes Thickness	0,02756	in
Impact Tubes Percentage	5	%
Tubes Material	Titanium	
Cleanliness Factor	0,9	

■ Results For Condenser Revamping

Cooling Water Flow	1166,72	cuft/s
Coolinw Water Increase Temperature	23,77	oF
Condensation Pressure	1,91	" Hg
Cooling Water Velocity In Tubes	6,59	ft/s
Number Of Tubes	67536	
Exchange Surface	737634	sqft
Tube Nest Pressure Drop	16,07	wftc
Exchange Coefficient	567,1	Btu/hofFt2

RESULTS SHEET 2/2